# CHAPTER - VI

# INHIBITION EFFICIENCY OF SELECTED POLYESTERS UNDER VARIOUS ACIDIC ENVIRONMENTS – A COMPARISON

#### **6.1 INTRODUCTION**

Owing to the unique properties of mild steel such as low cost, facile fabrication and strength, industrial dependence on mild steel has tremendously increased. When such mild steel experiences industrial exercises like pickling, cleaning of boilers or descaling, base metal dissolution arises which cannot be eliminated at any cause<sup>1</sup>. These process are mainly done to remove the impurities present on the metal surface. Though HF-HNO<sub>3</sub> mixture has the capability of removing scale and dust, its toxic environmental footprints like emission of nitrate effluents has paved the way for the usage of low cost mineral acids like H<sub>2</sub>SO<sub>4</sub>, HCl or H<sub>3</sub>PO<sub>4</sub> for a long time rather than organic acids. H<sub>2</sub>SO<sub>4</sub> commonly termed as universal chemical, has potential usage in diverse sectors like manufacturing of fertilisers, pharmaceuticals, gasolines, batteries, bleaching, steel manufacturing, refineries, electrolysis, sulphonation and regeneration of ion exchange resins. It is a very important commodity chemical, from which an industrial strength can be determined. Besides, its importance in metal industries for pickling process is endless due to its low cost.

HCl is a strong inorganic acid with a repository of industrial applications like pickling, oil and gas processing, chemical and petrochemical sectors<sup>2-4</sup> before subjecting to the process such as extrusion, rolling, galvanizing etc., Though H<sub>2</sub>SO<sub>4</sub> and HCl are strong acids, HCl is considered as a predominant one since its pickling rate is faster compared to H<sub>2</sub>SO<sub>4</sub>. Phosphoric acid (H<sub>3</sub>PO<sub>4</sub>) has gained important application in manufacture of fertilizers<sup>5</sup>. Its peculiar property of removing rust at a faster rate makes its role significant in cleaning expensive and precise items which hinders re-rusting process for a long period<sup>6</sup>. On the other hand, large scale industrial sectors utilises H<sub>3</sub>PO<sub>4</sub> for chemical/electrolytic polishing, etching, passivating and phosphating the surface of the metal<sup>7</sup>. Though H<sub>3</sub>PO<sub>4</sub> is a medium-strong acid, its affinity towards iron materials are high which has made researchers to think of a material that can minimise this affinity. Practically metals that exist in stable oxidised form has the tendency of reacting with the atmosphere to form metal oxides which is generally termed as rust. Eliminating this metal loss is too tedious whereas minimising this loss can be done effectively by using various strategies. In this regard, necessary measurements were taken to choose a low

cost method which is obviously an application of inhibitor, where the resulting compound fulfils the capability of getting oxidised, covering large surface, eco-friendly and safe handling which in turn minimises the metal dissolution<sup>8</sup>.

As an attempt, lot of research has been carried out to synthesise the inhibitors adopting various methodologies either to end with organic or inorganic compounds<sup>9-12</sup>. Various organic moieties synthesised were used as effective corrosion inhibitors for mild steel by **Hmimou** *et al.*,<sup>13</sup>, **Al-Senani**<sup>14</sup>, **Zaferani** *et al.*,<sup>15</sup>, **Desai** *et al.*,<sup>16</sup>, **Aziz** *et al.*,<sup>17</sup> **Divakara Shetty** *et al.*,<sup>18</sup> **Abdel Hameed** *et al.*,<sup>19</sup>. However cost, hazard nature and tedious synthetic procedures has minimised its usage in taking up the role of corrosion inhibitors. As a remedy, an alternate source of inhibitors were focussed which were of macromolecular size, possessing high molecular weight with a facile eco-friendly synthesis termed as polymers. As iron products decide the economy of industrial sectors, minimising its severity has to be stressed which has triggered us to evaluate the effect of linear polyesters PGAZ, PGSE and cardo polyesters MPOD, MPOU on mild steel protection. Compared to H<sub>2</sub>SO<sub>4</sub> and HCl, only a less effort has been contributed towards the study of metal protection under the influence of phosphoric acid. Owing to this, present chapter has been designed to compare the efficiencies under 0.5 M H<sub>2</sub>SO<sub>4</sub>, 1 M HCl and 0.3 M H<sub>3</sub>PO<sub>4</sub>.

#### **6.2 EXPERIMENTAL METHODS**

#### 6.2.1 Inhibitors

The inhibitors PGAZ, PGSE, MPOD and MPOU with maximum inhibiton efficiencies whose synthetic procedure are dealt in chapter II were chosen for the present discussion. The structure of the selected inhibitors are represented below.



#### 6.2.2 Materials

Mild steel couponsof desired dimensions were preferred for the present study. Various solutions of 0.5 M  $H_2SO_4$  1 M HCl and 0.3 M  $H_3PO_4$  were prepared by diluting analytical grade of respective acids with distille water.

# 6.2.3 Evaluation of metal protecting ability

To compare the inhibition efficiences of the selected inhibitors towards  $0.5 \text{ M H}_2\text{SO}_4$ , 1 M HCl and  $0.3 \text{ M H}_3\text{PO}_4$ , methodologes described in the earlier chapters were followed which could be outlined as shown.

Non- Electrochemical method – Mass loss method								
Metal	: Mild steel							
Major composition	: Fe (99.32%)							
Duration	: 3 hrs							
Electrolyte	: $0.5 \text{ M H}_2\text{SO}_4$ , 1 M HCl and $0.3 \text{ M H}_3\text{PO}_4$							
	Electrochemical methods							
Working electrode	: Mild steel rod with an exposed area of $0.785 \text{ cm}^2$							
Counter electrode	: Platinum electrode							
Reference electrode	: Calomel electrode							
Software	: Ivium compactstat							
Impedance measure	ments							
Frequency rar	nge : 10 KHZ to 0.01 HZ							
Amplitude	: 10 mV							
Polarisation measur	ements							
<ul><li>Potential rang</li></ul>	e : -200  to  +200  mV							
Scan rate	: 1 MV/sec							

### **6.3 RESULTS AND DISCUSSION**

#### 6.3.1 Evaluation of metal protecting ability

#### 6.3.1.1 Mass loss method

To analyse the fundamental response of an inhibitor in protecting the metal surface under aggressive medium, mass loss method can be adopted where the loss in mass of the specimens can be evaluated by immersing the mild steel specimens of standard dimensions in 100 ml test solution of 0.5 M H<sub>2</sub>SO<sub>4</sub> / 1 M HCl / 0.3 M H<sub>3</sub>PO<sub>4</sub> medium. From the data shown in **Tables 6.1-6.3**, it is observed that on increasing the concentration (10, 50, 100, 500, 000

ppm) of the inhibitors, a favourable increase in the surface coverage<sup>20</sup> on the mild steel surface was noticed thereby minimising the metal surface getting exposed to the acid medium. Comparing the weight loss data, at any concentration of the inhibitor, the inhibition efficiency was found to be in the order of HCl > H<sub>2</sub>SO<sub>4</sub> > H<sub>3</sub>PO<sub>4</sub> which could be attributed mainly based on the extent of adsorption of the inhibitor on the mild steel surface<sup>21</sup>. Out of the four inhibitors studied, the highest inhibition efficiency at optimised concentration of 1000 ppm obtained for MPOU and MPOD could be reasoned due to its + inductive effect of  $-CH_2$ - moieties along with the bulky structure and aromaticity that can involve  $\pi$ -electron cloud to interact with the metal surface thereby creating a better surface covering ability than the linear polyesters PGAZ and PGSE where aromaticity is not observed.

#### **6.3.1.2 Electrochemical impedance spectroscopy (EIS)**

From the Nyquist plots shown in Figs. 6.1-6.3, the response of the added polymers PGAZ, PGSE, MPOD and MPOU in 0.5 M H<sub>2</sub>SO<sub>4</sub> / 1 M HCl / 0.3 M H<sub>3</sub>PO<sub>4</sub> test medium can be clearly understood. In the case of uninhibited medium (blank) of all the three acids, the diameter of the semicircle was obviously less which insisted the lesser resistance to the metal dissolution in acidic media ie., the metal has undergone pronounced corrosion. On addition of selected concentrations (10, 100, 1000 ppm) of the inhibitor to the medium, successive increase in the diameter of the semicircle was observed with increased charge transfer resistance  $(R_{ct})$ as listed in Tables 6.4-6.6. The increase in R<sub>ct</sub> also suggested the formation of a protective barrier on the metal specimens thereby hindering the flow of ions into the medium<sup>22</sup>. On the other hand the double layer capacitance decreased with increase in the concentration of the inhibitors, which can be reasoned due to the replacement of already adsorbed water molecules on the metal surface by the added inhibitors where maximum replacement was favoured by MPOU resulting in higher inhibition efficiency of 93.24% in HCl medium. However the depression noticed in the semicircles might be due to the inhomogeneity of the metal surface or dispersion in frequency<sup>23</sup>. As suggested by most of the researchers, the obtained data were fitted within Randle's equivalent circuit which consisted of solution resistance (R<sub>s</sub>), charge transfer resistance (R<sub>ct</sub>) and double-layer capacitance (C<sub>dl</sub>). In the present discussion, R<sub>ct</sub> and C<sub>dl</sub> referred to the resistance and double layer capacitance of polymer-solution interface. Moreover corrosion inhibition process was found to be high in inhibited medium than the uninhibited ones which could be due to the addition of the inhibitors favouring a protective film on the metal surface thereby protecting the metal surface from getting exposed to the acidic

medium<sup>22</sup> or by decreasing surface heterogeneity due to the adsorption of inhibitors on the active sites<sup>24</sup>.

#### 6.3.1.3 Potentiodynamic polarisation technique

The influence of the inhibitor on the cathodic and anodic reactions were studied with the aid of potentiodynamic polarisation studies. The resulting polarisation parameters such as Tafel slopes ( $b_a$  and  $b_c$ ), corrosion current ( $I_{corr}$ ) and corrosion potential ( $E_{corr}$ ) corresponding to 0.5 M H<sub>2</sub>SO<sub>4</sub> / 1 M HCl / 0.3 M H<sub>3</sub>PO<sub>4</sub> are listed in Tables 6.7-6.9. Close observation of the data revealed that the Icorr values of uninhibited acidic medium decreased successively on addition of inhibitors revealing reduced corrosion process where a metal getting exposed to the acid medium is considerably reduced<sup>25</sup>. Minimum changes observed in the Tafel slopes does not change the metal dissolution mechanism. From Figs. 6.4-6.6, it can be seen that the addition of inhibitors PGAZ, PGSE, MPOD and MPOU affected both the cathodic and anodic curves. Observation of Tafel slopes did not show much variation implying that the added inhibitor has acted by simply blocking the surface and inducing inactivation towards corrosion<sup>26</sup>. Moreover the addition of inhibitor in the medium gets adsorbed in the metal/solution interface<sup>27</sup> thereby reducing the polarisation of the metal specimen ie., reducing the conversion of metal into metal ions. In addition the displacement in E<sub>corr</sub> value<sup>28</sup> observed was 45.1 mV, 38.7 mV and 39.1 mV under the influence of 0.5 M  $H_2SO_4$  / 1 M HCl / 0.3 M  $H_3PO_4$  which was less than 85mV thereby suggesting mixed type of inhibition favouring the reduction of both anodic metal dissolution and cathodic hydrogen evolution.

#### 6.3.1.4 Comparision of inhibition efficiency

Evaluation of the inhibition efficiency rendered by the inhibitors PGAZ, PGSE, MPOD and MPOU under various acidic environment like H<sub>2</sub>SO<sub>4</sub>, HCl and H<sub>3</sub>PO<sub>4</sub> has been made by weight loss, AC impedance and potentiodynamic polarisation techniques. All the measurements done revealed increased metal protecting ability on increasing the concentration of the inhibitors. Comparison of data presented in **Table 6.10**, showed increased inhibition efficiency for 1 M HCl test solution compared to 0.5 M H<sub>2</sub>SO<sub>4</sub> and 0.3 M H<sub>3</sub>PO<sub>4</sub> which could be reasoned due to the fact that Cl<sup>-</sup> have a stronger tendency to get adsorbed and has greater electrostatic influence on the inhibitor adsorption than SO<sub>4</sub><sup>2-</sup> and PO<sub>4</sub><sup>3-</sup> ions<sup>29,30</sup>. Thus the mode of inhibition lies in the order of HCl > H<sub>2</sub>SO<sub>4</sub> > H<sub>3</sub>PO<sub>4</sub> which indicates the acid anions as well as degree of protonation mainly influenced metal dissolution process<sup>31,32</sup>. This is additionally evident from the increased surface coverage of 0.9686 (1 M HCl) than 0.9298 (0.5 M H<sub>2</sub>SO<sub>4</sub>) and 0.8107 (0.3 M H<sub>3</sub>PO<sub>4</sub>) at 1000 ppm concentration of MPOU. As well the obtained C<sub>dl</sub>

values around 24.8 µF/cm<sup>2</sup> for HCl, 66.7 µF/cm<sup>2</sup> for sulphuric acid and 69.81 µF/cm<sup>2</sup> for phosphoric acid also supported the same. When a mild steel specimen is immersed in a test solution of 1 M HCl / 0.5 M H<sub>2</sub>SO<sub>4</sub> / 0.3 M H<sub>3</sub>PO<sub>4</sub> comparatively Cl<sup>-</sup> ions being smaller in size and its lesser degree of hydration enables it to get strongly adsorbed first on the mild steel surface creating excess negative charge<sup>33,34</sup> than SO<sub>4</sub><sup>2-</sup> and PO<sub>4</sub><sup>3-</sup> ions which possess lower degree of hydration rendering weaker mode of adsorption. From the results obtained, it can be suggested that the added inhibitor could either replace already adsorbed Cl<sup>-</sup> ions or it could favour a synergistic mode of inhibition where the inhibitor gets adsorbed on Fe-Cl surface<sup>35</sup>. The increased inhibition favoured under HCl medium can be reasoned due to the joint adsorption where the chloride ion has worked along with the inhibitor. It is a general mechanism that the mild steel immersed in acidic medium gets positively charged which creates an electrostatic repulsion between the protonated inhibitor molecules. Thus in the present study, among the existing anions  $Cl^{-}$ ,  $SO_4^{2-}$  and  $PO_4^{3-}$  ions  $Cl^{-}$  possess the capability of adsorbing more cations<sup>36</sup> than  $SO_4^{2-}$  and  $PO_4^{3-}$  ions favouring the inhibition efficiency in the order of  $HCl > H_2SO_4 > H_3PO_4$ . Also major factors like functional groups and molecular structure<sup>37</sup> also contributes towards the inhibition phenomena where a single polymeric molecule has the capability of displacing more water molecules than organic compounds<sup>38</sup>. The present discussion also revealed the same favouring higher inhibition efficiency for MPOU due to aromaticity, bulky structure and electron donating ability of oxygen atoms<sup>39,40</sup> than PGSE of lower inhibition efficiency because of the absence of the aromatic electron cloud.

## **6.4 CONCLUSIONS**

From the above comparison studies, the following conclusions were drawn.

- (ix) Mass loss method favoured highest inhibition efficiency of 96.86 % for MPOU in HCl medium.
- (x) Efficiencies obtained from AC impedance and polarisation measurements were in good agreement with each other.
- (xi) The comparison study revealed the inhibition of mild steel specimens in the order of  $1 \text{ M HCl} > 0.5 \text{ M H}_2\text{SO}_4 > 0.3 \text{ M H}_3\text{PO}_4$ .

#### **6.5 REFERENCES**

- 1. A.F.S. Abdul Rahiman, S. Sethumanickam, Arabian J. Chem., 10 (2017) S3358–S3366.
- C.B. Verma, M.A. Quraishi, E.E. Ebenso, Int. J. Electrochem. Sci., 9 (2014) 5507 – 5519.
- 3. G. Karthik, M. Sundaravadivelu, Egypt. J. Pet., 25 (2016) 183–191.
- 4. A.J.A. Nasser, M.A. Sathiq, Arabian J. Chem., 9 (2016) S691–S698.
- 5. E. Khamis, M.A. Ameer, N.M. Alandis, C. Al-senai, Corros. Sci., 56(2) (2000) 127-138.
- 6. V.S. Muralidharan, K.S. Rajagopalan, Corros. Sci., 19 (1979) 199–207.
- 7. X. Li, S. Deng, H. Fu, Corros. Sci., 55 (2012) 280–288.
- T. Douadi, H. Hamani, D. Daoud, M. Al-Noaimi, S. Chafaa, J. Taiwan. Inst. Chem. E., 71 (2017) 388-404.
- J.N. Asegbeloyin, P.M. Ejikeme, L.O. Lukman, A.S. Adekunle, E.E. Ebenso, Mater., 8(6) (2015) 2918-2934.
- 10. A.Y.I. Rubaye, H.T. Abdulsahib, A.A. Abdulwahid, Encaps. Ads. Sci., 5 (2015) 155-164.
- H. Elmsellem, A. Aouniti, Y. Toubi, H. Steli, M. Elazzouzi, S. Radi, B. Elmahi,
  Y. El Ouadi, A. Chetouani, B. Hammouti, Der pharma chem., 7(7) (2015) 353-364.
- 12. L. Khandelwal, C.B. Verma, M.A. Quraishi, J. Mater. Environ. Sci., 6 (2015) 810-817.
- J. Hmimou, A. Rochdi, R. Touir, M.E. Touhami, E.H. Rifi, A. El Hallaoui, A. Anouar,
  D. Chebab, J. Mater. Environ. Sci., 3 (3) (2012) 543-550.
- 14. G.M. Al-Senani, Int. J. Electrochem. Sci.., 11 (2016) 291 302.
- 15. S.H. Zaferani, M.R. Shishesaz, J. Pet. Environ. Biotechnol, 5(4) (2014) 1-5.
- 16. P.S. Desai, N.S. Indorwala, Int. J. Curr. Microbiol. Appl. Sci., 4(2) (2015) 928-938.
- A. Md. Aziz, Z.H. Md. Khan, S. Mst Khatun, R. Md. Hasan, Aceh Int. J. Sci. Technol., 3(1) (2014) 19-26.
- 18. S.D. Shetty, N. Shetty, Int. J. Technol., 5 (2016) 755-766.
- 19. R.S.A. Hameed, Portugaliae Electrochim. Acta., 29(4) (2011) 273-285.
- 20. I.A. Akpan, N.A.O. Offiong, Int. J. corros., 2013 (2013) 1-5.
- 21. A. Popova, Corros. Sci., 49 (2007) 2144-2158.
- 22. P. Muthirulan, N. Rajendran, Surf. Coat. Technol., 206 (2012) 2072–2078.
- 23. R. Karthikaiselvi, S. Subhashini, J Assn Arab Univ Basic Appl Sci., 16 (2014) 74-82.
- 24. R.A. Ahmed, R. A. Farghali, A.M. Fekry, Int. J. Electrochem. Sci., 7 (2012) 7270 7282.

- 25. R. Geethanjali, S. Subhashini, Chem Sci Trans., 2(4) (2013) 1148-1159.
- M.M. El-Deeb, S.M. Sayyah, S.S. Abd El-Rehim, S.M. Mohamed, Arabian J. Chem., 8 (2015) 527–537.
- 27. M. Mobin, M. Rizvi, Carbohydr. Polym., 136 (2016) 384-393.
- 28. Y. Yi, G. Liu, Z. Jin, D. Feng, Int. J. Electrochem. Sci., 8 (2013) 3540 3550.
- 29. Q. H. Cai, Y. K. Shan, B. Lu, X. H. Yuan, Corros., 49 (1993) 486 490,
- F. Bentiss, M. Traisnel, N. Chaibi, B. Mernari, H. Vezin, M. Lagrenee, Corros. Sci., 44 (2016) 2271 – 2289.
- 31. E.E. Oguzie, Port. Electrochim. Acta., 26 (2008) 303-314.
- 32. M. Lashgari, M.R. Arshadi, M.J. Biglar, J. Iran. Chem. Soc., 7(2) (2010) 478-486.
- 33. L. Tang, X. Li, L. Lin, G. Mu, G. Liu, Mater. Chem. Phys., 97(2-3) (2006) 301-307.
- 34. A. Yurt, A. Balaban, S.U. Kandemir, G. Bereket, B. Erk, Mater. Chem. Phys., 85(2–3) (2004) 420–426.
- 35. S. S. Abd El Rehim, S. M. Sayyah, M. M. El-Deeb, S. M. Kamal, R. E. Azooz, Int. J. Ind. Chem., 7 (2016) 39–52.
- 36. X. Li, S. Deng, H. Fu, X. Xie, Corros. Sci., 78 (2014) 29-42.
- N. Anusuya, J. Saranya, P. Sounthari, A. Zarrouk, S. Chitra, J. Mol. Liq., 225 (2017) 406–417.
- 38. M.A. Amin, S.S. Abd EI-Rehim, E.E.F. El-Sherbini, O.A. Hazzazi, M.N. Abbas, Corros. Sci., 51 (2009) 658–667.
- A. Bellaouchou, B. Kabkab, A. Guenbour, A. Ben Bachir, Prog. Org. Coat., 41 (2001) 121–127.
- 40. G. Thenmozhi, P. Arockiasamy, G. Mohanraj, R. Jaya Santhi, Portugaliae Electrochim. Acta., **32(5)** (2014) 355-367.

Surface Weight Inhibition Corrosion Name of the Conc. loss Efficiency Coverage rate Inhibitor (ppm) ( g cm<sup>-2</sup> hr<sup>-1</sup>) **(g)** (%) (θ) 19.97 **BLANK** 0.2015 \_ -10 0.0976 51.59 0.5159 9.67 50 0.0934 53.66 9.25 0.5366 PGAZ 100 0.0929 53.88 9.21 0.5388 500 0.0756 62.49 0.6249 7.49 1000 0.0645 67.97 0.6797 6.40 10 0.0956 52.55 0.5255 9.48 50 54.18 9.15 0.0923 0.5418 54.38 9.11 PGSE 100 0.0919 0.5438 500 0.0723 64.14 7.16 0.6414 1000 0.0451 77.63 4.47 0.7763 10 6.92 0.0698 65.36 0.6536 50 6.05 0.0610 69.71 0.6971 100 5.54 0.0559 72.24 0.7224 **MPOD** 500 3.26 0.0329 83.69 0.8369 1000 1.63 0.0164 91.85 0.9185 10 6.18 0.0624 69.04 0.6904 50 5.31 0.0536 73.4 0.734 100 4.75 0.0480 76.19 0.7619 MPOU 500 1.99 0.0201 90.01 0.9001 1000 0.76 0.0141 92.98 0.9298

Table 6.1 Inhibition efficiencies of various concentrations of the polyesters for corrosionof mild steel in 0.5 M H2SO4 by weight loss measurement at 303 K

Weight Inhibition Corrosion Surface Name of Conc. loss Efficiency Coverage rate the (ppm)  $(g cm^{-2} hr^{-1})$ **(g)** (%) Inhibitor **(θ)** 0.2216 21.96 Blank \_ --10 0.0877 60.41 0.6041 8.69 50 0.0816 63.18 0.6318 8.09 PGAZ 100 0.0704 68.22 0.6822 6.98 500 0.0592 73.29 0.7329 5.87 1000 0.0510 76.98 0.7698 5.06 0.0704 10 68.23 0.6823 6.98 50 0.0683 69.19 0.6919 6.77 100 0.0612 72.38 0.7238 6.07 PGSE 500 0.0460 79.25 0.7925 4.56 1000 0.0332 85.03 0.8503 3.29 76.14 10 0.0529 0.7614 5.24 50 0.0407 81.65 0.8165 4.03 **MPOD** 100 0.0337 84.81 0.8481 3.34 500 0.0238 89.24 0.8924 2.36 1000 0.0172 92.22 0.9222 1.71 10 79.85 4.43 0.0447 0.7985 3.54 50 0.0358 83.86 0.8386 **MPOU** 100 0.0285 87.13 0.8713 2.83 500 0.0163 92.64 0.9264 1.62 1000 0.0070 96.86 0.9686 0.69

Table 6.2 Inhibition efficiencies of various concentrations of the polyesters for corrosionof mild steel in 1 M HCl by weight loss measurement at 303 K

Table 6.3 Inhibition efficiencies of various concentrations of the polyesters for corrosionof mild steel in 0.3 M H<sub>3</sub>PO4 by weight loss measurement at 303 K

Name of the Inhibitor	Conc. (ppm)	Weight loss (g)	Inhibition Efficiency (%)	Surface Coverage (θ)	Corrosion rate (g cm <sup>-2</sup> hr <sup>-1</sup> )
Blank	-	0.2138	_	-	21.19
	10	0.1201	43.81	0.4381	11.91
	50	0.1193	44.21	0.4421	11.82
PGAZ	100	0.1178	44.9	0.449	11.67
	500	0.1110	48.06	0.4806	11.01
	1000	0.1013	52.61	0.5261	10.04
	10	0.1169	45.32	0.4532	11.59
	50	0.1129	47.18	0.4718	11.19
PGSE	100	0.1077	49.63	0.4963	10.67
	500	0.0935	56.25	0.5625	9.27
	1000	0.0833	61.04	0.6104	8.26
	10	0.0966	54.84	0.5484	9.57
	50	0.0817	61.8	0.618	8.09
MPOD	100	0.0787	63.21	0.6321	7.80
	500	0.0657	69.25	0.6925	6.52
	1000	0.0506	76.33	0.7633	5.02
	10	0.0852	60.15	0.6015	8.44
	50	0.0764	64.25	0.6425	7.57
MPOU	100	0.0654	69.43	0.6943	6.48
	500	0.0528	75.32	0.7532	5.23
	1000	0.0405	81.07	0.8107	4.01

Name of the inhibitor	Conc. (ppm)	R <sub>ct</sub> (ohm cm <sup>2</sup> )	C <sub>dl</sub> (µF/cm <sup>2</sup> )	Inhibition efficiency (%)
BLANK	-	15.8	21.5	-
	10	30.1	18.7	47.51
PGAZ	100	35.2	18.4	55.11
	1000	43.6	14.9	63.76
PGSE	10	30.9	19.8	48.87
	100	37.3	18.5	57.64
	1000	48.5	16.8	67.42
	10	32.91	29.5	51.99
MPOD	100	46.14	18.3	65.76
	1000	88.76	16.7	82.20
MPOU	10	35.67	36.1	55.71
	100	49.95	23.1	68.37
	1000	101.86	19.2	84.49

Table 6.4 AC-impedance parameters for corrosion of mild steel for selectedconcentrations of the polyesters in 0.5 M H2SO4

Name of the inhibitor	Conc. (ppm)	R <sub>ct</sub> (ohm cm <sup>2</sup> )	$C_{dl}$ ( $\mu$ F/cm <sup>2</sup> )	Inhibition efficiency (%)
Blank	-	17.8	24.8	-
	10	43.15	41.1	58.74
PGAZ	100	48.95	38.3	63.63
	1000	72.82	35.3	75.55
	10	48.89	32.4	63.59
PGSE	100	51.67	30.1	65.55
	1000	95.63	29.6	81.38
	10	63.25	30.08	71.85
MPOD	100	96.01	26.84	81.46
	1000	180.01	23.20	90.11
	10	108.15	26.4	83.54
MPOU	100	149.13	23.3	88.06
	1000	263.18	23.9	93.24

Table 6.5 AC-impedance parameters for corrosion of mild steel for selectedconcentrations of the polyesters in 1 M HCl

Name of the inhibitor	Conc. (ppm)	R <sub>ct</sub> (ohm cm <sup>2</sup> )	$C_{dl}$ ( $\mu F/cm^2$ )	Inhibition efficiency (%)
Blank	-	14.87	69.81	-
	10	25.24	46.9	41.08
PGAZ	100	26.32	43.5	43.50
	1000	29.98	42.1	50.40
PGSE	10	26.51	36.7	43.91
	100	26.89	35.8	44.70
	1000	34.25	29.8	56.58
	10	30.01	30.6	50.44
MPOD	100	39.22	29.7	62.08
	1000	48.94	24.1	69.61
MPOU	10	33.81	29.8	56.01
	100	40.13	26.5	62.94
	1000	53.82	22.1	72.37

Table 6.6 AC-impedance parameters for corrosion of mild steel for selectedconcentrations of the polyesters in 0.3 M H<sub>3</sub>PO<sub>4</sub>

Name of the inhibitor	Conc.	Tafel slopes (mV/dec)		-E <sub>corr</sub> (mV)	Icorr	Inhibition efficiency
	(ppm)	ba	bc	vs SCE	(μA/cm <sup>-</sup> )	(%)
BLANK	-	63	153	476.9	896.52	
	10	53	139	487.4	468.56	47.74
PGAZ	100	57	127	493.2	435.69	51.40
	1000	68	118	522	410.25	54.24
PGSE	10	63	136	498.8	440.28	50.89
	100	62	126	492.5	415.28	53.68
	1000	69	111	517.4	342.23	61.83
	10	64	165	473.1	364.88	59.30
MPOD	100	59	161	466.9	305.27	65.95
	1000	57	163	475.8	129.73	85.53
MPOU	10	54	164	476.3	360.31	59.81
	100	52	159	475.7	295.49	67.04
	1000	50	167	474.7	159.04	82.26

Table 6.7 Potentiodynamic polarisation parameters for corrosion of mild steel withselected concentration of the polyesters in 0.5 M H2SO4

Nome of		Tafel slopes		-Ecorr		Inhibition	
the	Conc.	(mV/dec)		(mV)	Icorr	officioney	
uit inhihitan	(ppm)	ba	bc	vs	(µA/cm <sup>2</sup> )		
Inhibitor				SCE		(%0)	
Blank	-	57	163	536.7	660.69	-	
	10	67	157	561.5	351.42	46.81	
PGAZ	100	64	143	549.4	322.94	51.12	
	1000	59	137	531.1	288.52	56.33	
PGSE	10	63	117	551.9	335.56	49.21	
	100	59	127	552	295.06	55.34	
	1000	61	126	536.7	233.02	64.73	
	10	62	131	548.1	304.37	53.93	
MPOD	100	57	125	575.1	255.55	61.32	
	1000	57	125	575.4	172.57	73.88	
	10	57	163	536.3	279.93	57.63	
MPOU	100	58	153	543.5	237.18	64.10	
	1000	60	138	557.1	102.27	84.52	

Table 6.8 Potentiodynamic polarisation parameters for corrosion of mild steel withselected concentration of the polyesters in 1 M HCl

Name of the	Conc.	Tafel slopes (mV/dec)		-E <sub>corr</sub> (mV)	Icorr	Inhibition efficiency
inhibitor	(ppm)	ba	bc	vs SCE	(µA/cm <sup>2</sup> )	(%)
Blank	-	79	155	597.5	598.27	-
	10	87	148	605.4	360.09	39.81
PGAZ	100	82	142	593.4	350.46	41.42
	1000	73	147	582.3	331.32	44.62
PGSE	10	78	154	599.1	340.95	43.01
	100	79	149	591.2	338.56	43.41
	1000	79	156	587.7	297.22	50.32
	10	85	151	609.3	324.14	45.82
MPOD	100	83	144	625.7	292.01	51.19
	1000	71	168	636.6	252.17	57.85
MPOU	10	77	156	605.1	304.45	49.11
	100	79	147	608.1	267.78	55.24
	1000	74	158	627.4	210.17	64.87

Table 6.9 Potentiodynamic polarisation parameters for corrosion of mild steel withselected concentration of the polyesters in 0.3 M H<sub>3</sub>PO<sub>4</sub>

Tachniques used	Acid	Conc.		Name of the inhibitor			
i echniques useu	medium	(ppm)	PGAZ	PGSE	MPOD	MPOU	
	0.5 M	10	51.59	52.55	65.36	69.04	
		50	53.66	54.18	69.71	73.4	
	U.S M U.SO	100	53.88	54.38	72.24	76.19	
	112504	500	62.49	64.14	83.69	90.01	
		1000	67.97	77.63	91.85	92.98	
		10	60.41	68.23	76.14	79.85	
	1 M	50	63.18	69.19	81.65	83.86	
Weight loss		100	68.22	72.38	84.81	87.13	
	IICI	500	73.29	79.25	89.24	92.64	
		1000	76.98	85.03	92.22	96.86	
		10	43.81	45.32	54.84	60.15	
	0.2 M	50	44.21	47.18	61.8	64.25	
	0.3 M H <sub>3</sub> PO <sub>4</sub>	100	44.9	49.63	63.21	69.43	
		500	48.06	56.25	69.25	75.32	
		1000	52.61	61.04	76.33	81.07	
	0.5 M H <sub>2</sub> SO <sub>4</sub>	10	47.51	48.87	51.99	55.71	
		100	55.11	57.64	65.76	68.37	
AC impedance		1000	63.76	67.42	82.20	84.49	
	1 M	10	58.74	63.59	71.85	74.98	
	HCl	100	63.63	65.55	81.46	85.18	
		1000	75.55	81.38	90.11	93.46	
	0.2 M	10	41.08	43.91	50.44	56.01	
	U.3 M H2PO4	100	43.50	44.70	62.08	62.94	
	1131 04	1000	50.40	56.58	69.61	72.37	
	0.5 M	10	47.74	50.89	59.30	59.81	
	H2SO4	100	51.40	53.68	65.95	67.04	
	112004	1000	54.24	61.83	85.53	82.26	
Potentiodynamic	1 M	10	46.81	49.21	53.93	57.63	
polarisation	HC1	100	51.12	55.34	61.32	64.10	
	nei	1000	56.33	64.73	73.88	84.52	
		10	39.81	43.01	45.82	49.11	
	0.3 M	100	41.42	43.41	51.19	55.24	
	H <sub>3</sub> PO <sub>4</sub>	1000	44.62	50.32	57.85	64.87	

Table 6.10 Comparison of inhibition efficiencies in 0.5 M H<sub>2</sub>SO<sub>4</sub>, 1 M HCl and 0.3 M H<sub>3</sub>PO<sub>4</sub> by weight loss, AC impedance and polarisation measurements



Fig. 6.1 Nyquist plot for mild steel in 0.5 M  $\mathrm{H}_2\mathrm{SO}_4$  for selected concentrations



Fig. 6.2 Nyquist plot for mild steel in 1M HCl for selected concentrations



Fig. 6.3 Nyquist plot for mild steel in 0.3 M H<sub>3</sub>PO<sub>4</sub> for selected concentrations



Fig. 6.4 Polarization curves for mild steel in 0.5 M H<sub>2</sub>SO<sub>4</sub> for selected concentrations



Fig. 6.5 Polarization curves for mild steel in 1M HCl for selected concentrations



Fig. 6.6 Polarization curves for mild steel in 0.3 M H<sub>3</sub>PO<sub>4</sub> for selected concentrations